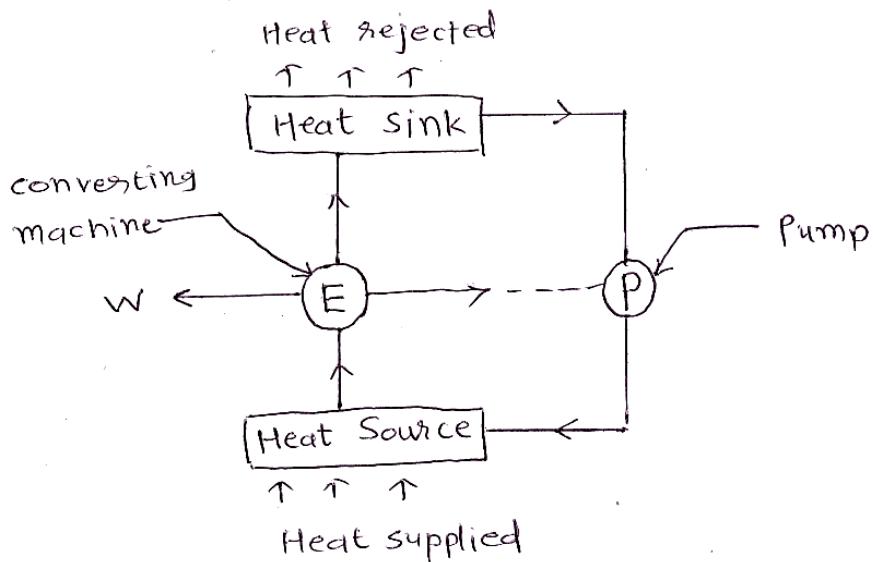


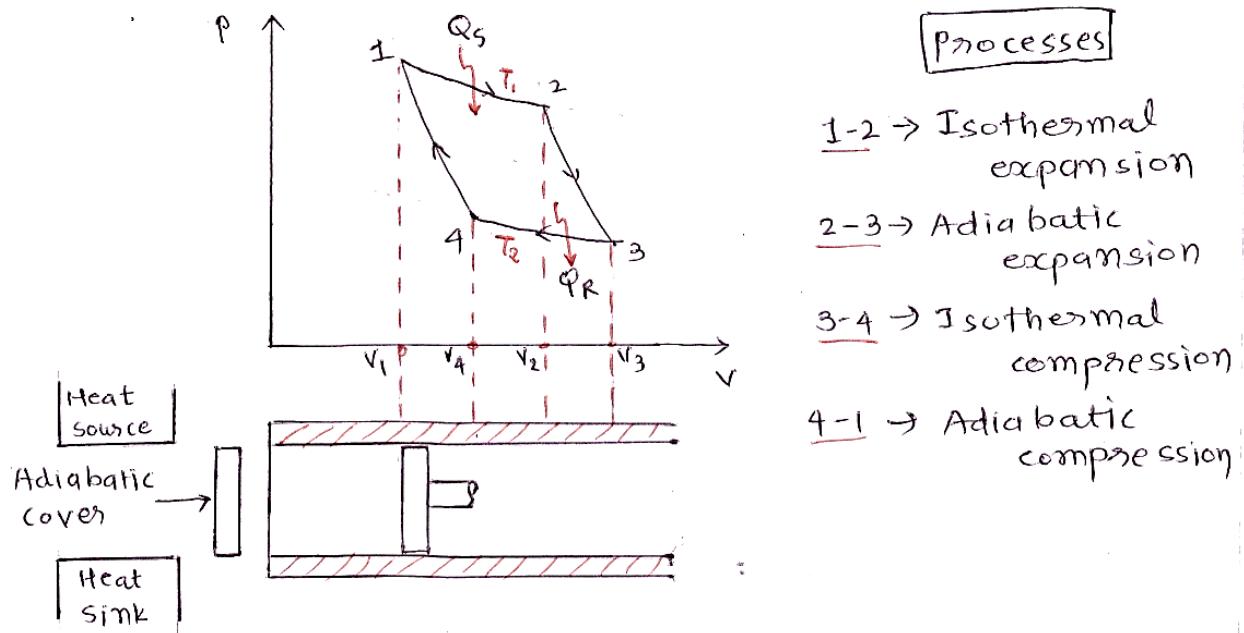
Chapter – 5 Heat Engines

Heat engine :- It is a device which converts chemical energy of fuel into heat energy and this heat energy is used to produce work



⇒ Various Heat engine cycles

① Carnot cycle



→ Efficiency of Carnot cycle

* Heat supplied during process (1-2)

$$Q_S = P_1 V_1 \ln \frac{V_2}{V_1} = m R T_1 \ln \frac{V_2}{V_1} \quad \dots \textcircled{1}$$

* Heat rejected during process (3-4)

$$Q_R = P_3 V_3 \ln \frac{V_4}{V_3} = m R T_2 \ln \frac{V_4}{V_3} \quad \dots \textcircled{2}$$

Now, Take $\gamma = \text{ratio of expansion} = V_2/V_1$

= ratio of compression = V_4/V_3

so, from eqⁿ ① and ②

$$Q_S = m R T_1 \ln \gamma \quad \text{and} \quad Q_R = m R T_2 \ln \gamma$$

so, Work done $W = Q_S - Q_R$

$$= m R T_1 \ln(\gamma) - m R T_2 \ln(\gamma)$$

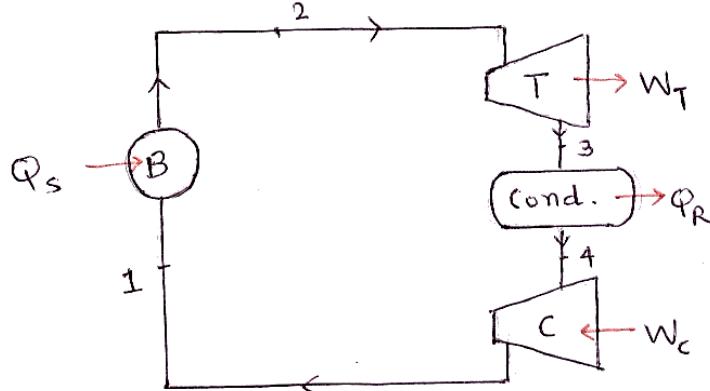
$$= m R (T_1 - T_2) \cdot \ln(\gamma)$$

Now, Efficiency $\eta = \frac{\text{output}}{\text{Input}} = \frac{\text{Work done}(W)}{\text{Heat supplied}(Q_S)}$

$$\eta = \frac{m R (T_1 - T_2) \cdot \ln(\gamma)}{m R T_1 \cdot \ln(\gamma)}$$

$$\boxed{\eta = \frac{T_1 - T_2}{T_1}}$$

② Cannot vapour cycle

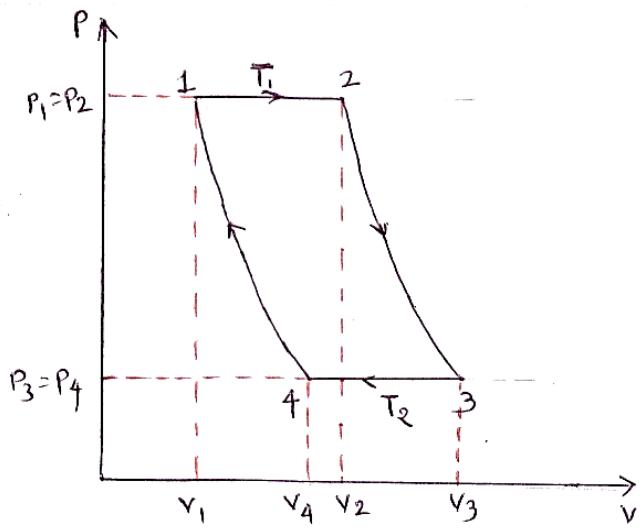


B = Boiler

T = Turbine

cond. = condenser

C = compressor



Processes

1-2 → Isothermal expansion

2-3 → Adiabatic expansion

3-4 → Isothermal compression

4-1 → Adiabatic compression

Here, Work

$$W_T = h_2 - h_3$$

$$W_C = h_1 - h_4$$

Heat

$$Q_S = h_2 - h_1$$

$$Q_R = h_3 - h_4$$

$$\text{Now, efficiency } \eta = \frac{\text{output}}{\text{Input}} = \frac{W}{Q_S}$$

$$= \frac{Q_S - Q_R}{Q_S}$$

Now, $Q = T \Delta S$ where $\Delta S = \text{change in entropy}$

$$\text{so, } Q_S = T_1(S_2 - S_1) \text{ and } Q_R = T_2(S_3 - S_4)$$

Also, $\Delta S = 0$ for Reversible Adiabatic process

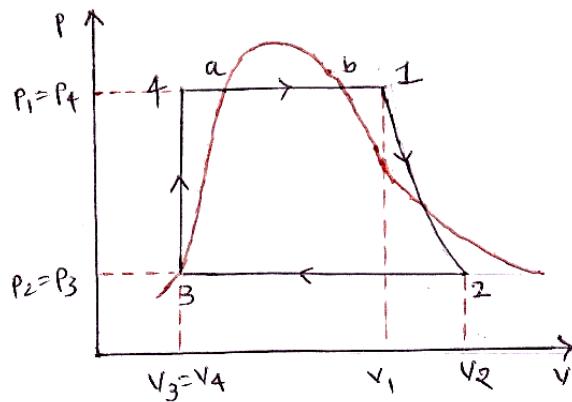
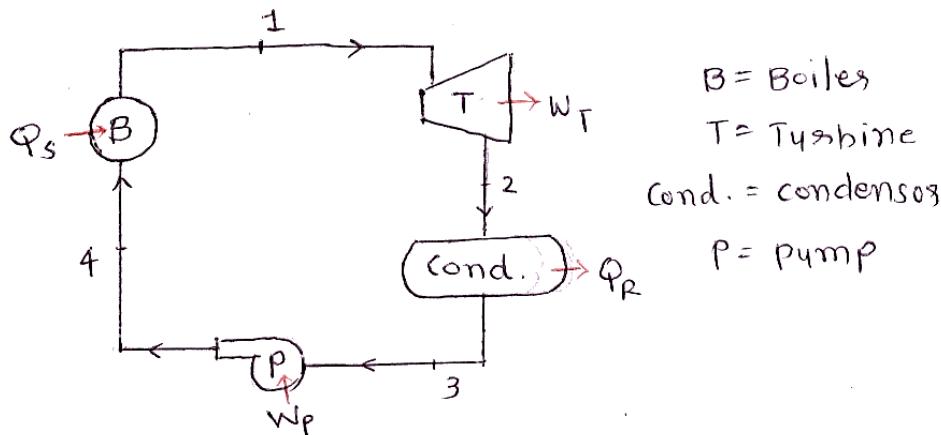
∴ for process 2-3 $\Rightarrow S_2 = S_3$

and for process 4-1 $\Rightarrow S_4 = S_1$

$$\begin{aligned} \therefore \eta &= \frac{Q_S - Q_R}{Q_S} \\ &= \frac{T_1(S_2 - S_1) - T_2(S_3 - S_4)}{T_1(S_2 - S_1)} \\ &= \frac{T_1(S_2 - S_1) - T_2(S_2 - S_1)}{T_1(S_2 - S_1)} \quad [\because S_2 = S_3 \text{ & } S_4 = S_1] \end{aligned}$$

$$\eta = \frac{T_1 - T_2}{T_1}$$

③ Rankine cycle



Work

$$W_T = h_1 - h_2$$

$$W_P = h_4 - h_3$$

Heat

$$Q_S = h_1 - h_4$$

$$Q_R = h_2 - h_3$$

$$\begin{aligned} \text{Efficiency } \eta &= \frac{\text{output}}{\text{Input}} = \frac{\text{Work done}}{\text{Heat supplied}} \\ &= \frac{Q_S - Q_R}{Q_S} \\ &= \frac{(h_1 - h_4) - (h_2 - h_3)}{(h_1 - h_4)} \quad \text{--- (1)} \end{aligned}$$

$$\boxed{\eta_L = 1 - \frac{h_2 - h_3}{h_1 - h_4}}$$

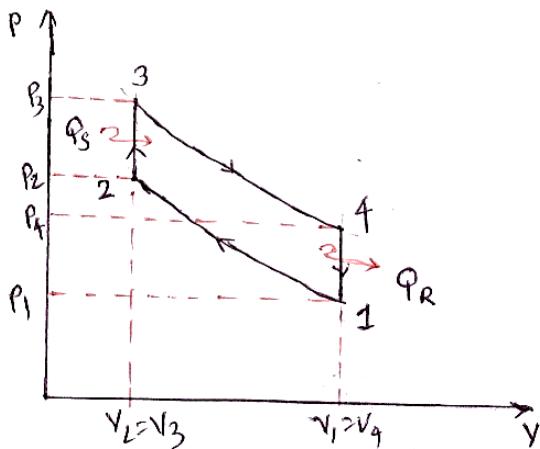
from eqⁿ (1)

$$\eta = \frac{h_1 - h_4 - h_2 + h_3}{h_1 - h_4} = \frac{(h_1 - h_2) - (h_4 - h_3)}{(h_1 - h_4)}$$

But, $h_4 - h_3 = \text{pump work } (W_P)$ which is very small and can be neglected so,

$$\boxed{\eta = \frac{h_1 - h_2}{h_1 - h_4}}$$

* Otto cycle :-



Process

- 1-2 \rightarrow Adiabatic
- 2-3 \rightarrow constant volume
- 3-4 \rightarrow Adiabatic
- 4-1 \rightarrow constant volume

Heat :- for process 2-3 $Q_S = m \cdot C_V (T_3 - T_2)$

for process 4-1 $Q_R = m \cdot C_V (T_4 - T_1)$

$$\begin{aligned} \text{Now, Efficiency } \eta &= \frac{\text{output}}{\text{Input}} = \frac{\text{Work done (W)}}{\text{Heat supplied (Qs)}} \\ &= \frac{Q_S - Q_R}{Q_S} \\ &= \frac{m \cdot C_V (T_3 - T_2) - m \cdot C_V (T_4 - T_1)}{m \cdot C_V (T_3 - T_2)} \end{aligned}$$

$$\eta = 1 - \frac{T_4 - T_1}{T_3 - T_2} \quad \dots \quad (1)$$

Consider

$$\text{Adiabatic process 1-2} \rightarrow \frac{T_2}{T_1} = \left(\frac{V_1}{V_2} \right)^{\gamma-1}$$

$$\therefore T_2 = T_1 \cdot r^{\gamma-1} \quad (2)$$

compression ratio

$$r = \frac{V_1}{V_2} = \frac{V_4}{V_3}$$

$$\begin{aligned} \text{Adiabatic process 3-4} \rightarrow \frac{T_3}{T_4} &= \left(\frac{V_4}{V_3} \right)^{\gamma-1} \\ \therefore T_3 &= T_4 \cdot r^{\gamma-1} \quad (3) \end{aligned}$$

from eqⁿ (1), (2) and (3)

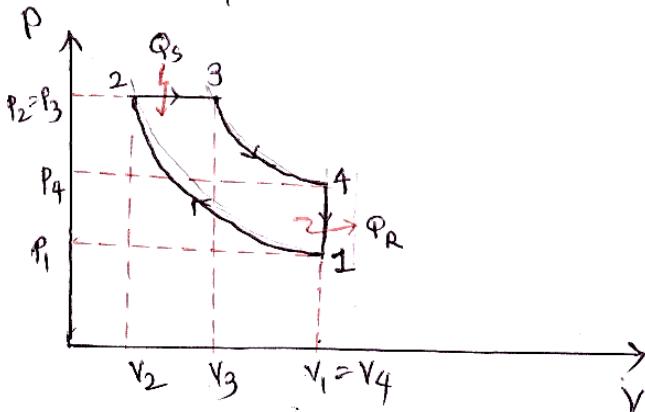


$$\eta = 1 - \frac{T_4 - T_1}{T_4 \cdot \gamma^{\gamma-1} - T_1 \cdot \gamma^{\gamma-1}}$$

$$= 1 - \frac{(T_4 - T_1)}{\gamma^{\gamma-1} (T_4 - T_1)}$$

$$\therefore \boxed{\eta = 1 - \frac{1}{\gamma^{\gamma-1}}}$$

* Diesel cycle :-



Process

1-2 \rightarrow Adiabatic

2-3 \rightarrow constant pressure

3-4 \rightarrow Adiabatic

4-1 \rightarrow constant volume

Heat Transfer :-

$$\text{for process } 2-3 \quad Q_s = m \cdot C_p (T_3 - T_2)$$

$$\text{for process } 4-1 \quad Q_R = m \cdot C_v (T_4 - T_1)$$

$$\text{Now, efficiency } \eta = \frac{\text{output}}{\text{Input}} = \frac{\text{Work done}(W)}{\text{Heat supplied}(Q_s)}$$

$$= \frac{Q_s - Q_R}{Q_s}$$

$$= \frac{m \cdot C_p (T_3 - T_2) - m \cdot C_v (T_4 - T_1)}{m \cdot C_p (T_3 - T_2)}$$

$$= 1 - \frac{T_4 - T_1}{\gamma (T_3 - T_2)} \quad \dots \textcircled{1}$$

Here, compression ratio, $\gamma = V_1/V_2$

cutoff ratio, $s = V_3/V_2$ and

$$\text{expansion ratio} = V_4/V_3 = \frac{V_4/V_2}{V_2/V_3} = \frac{\gamma}{s}$$

consider,

Adiabatic process 1-2 $\rightarrow \frac{T_2}{T_1} = \left(\frac{V_1}{V_2}\right)^{\gamma-1}$

$$T_2 = T_1 \cdot \cancel{s}^{\gamma-1}$$

constant pressure process

$$2-3 \rightarrow \frac{T_3}{T_2} = \frac{V_3}{V_2}$$

$$\therefore T_3 = \frac{T_2 \cdot s}{\cancel{s}^{\gamma-1}}$$
$$\therefore T_3 = T_1 \cdot \cancel{s}^{\gamma-1} \cdot s$$

Adiabatic process 3-4 $\rightarrow \frac{T_4}{T_3} = \left(\frac{V_3}{V_4}\right)^{\gamma-1}$

$$T_4 = T_3 \cdot \left(\frac{s}{\cancel{s}^{\gamma-1}}\right)^{\gamma-1}$$
$$= T_1 \cdot \cancel{s}^{\gamma-1} \cdot s \cdot \frac{s^{\gamma-1}}{\cancel{s}^{2\gamma-2}}$$

$$T_4 = T_1 \cdot s^\gamma$$

Put the values of T_2 , T_3 & T_4 in eqⁿ ①

$$\therefore \eta = 1 - \frac{T_1 \cdot s^\gamma - T_1}{\gamma [T_1 \cdot \cancel{s}^{\gamma-1} \cdot s - T_1 \cdot \cancel{s}^{\gamma-1}]}$$

$$= 1 - \frac{T_1 (s^\gamma - 1)}{\gamma \cdot \cancel{s}^{\gamma-1} \cdot T_1 (s-1)}$$

$$\boxed{\eta = 1 - \frac{1}{\cancel{s}^{\gamma-1}} \left[\frac{s^\gamma - 1}{\gamma (s-1)} \right]}$$